



ZoneFlow Reactor Technologies, LLC

Innovative ZoneFlow™ Technology Offers Breakthrough Solutions in Refinery Hydrogen Generation

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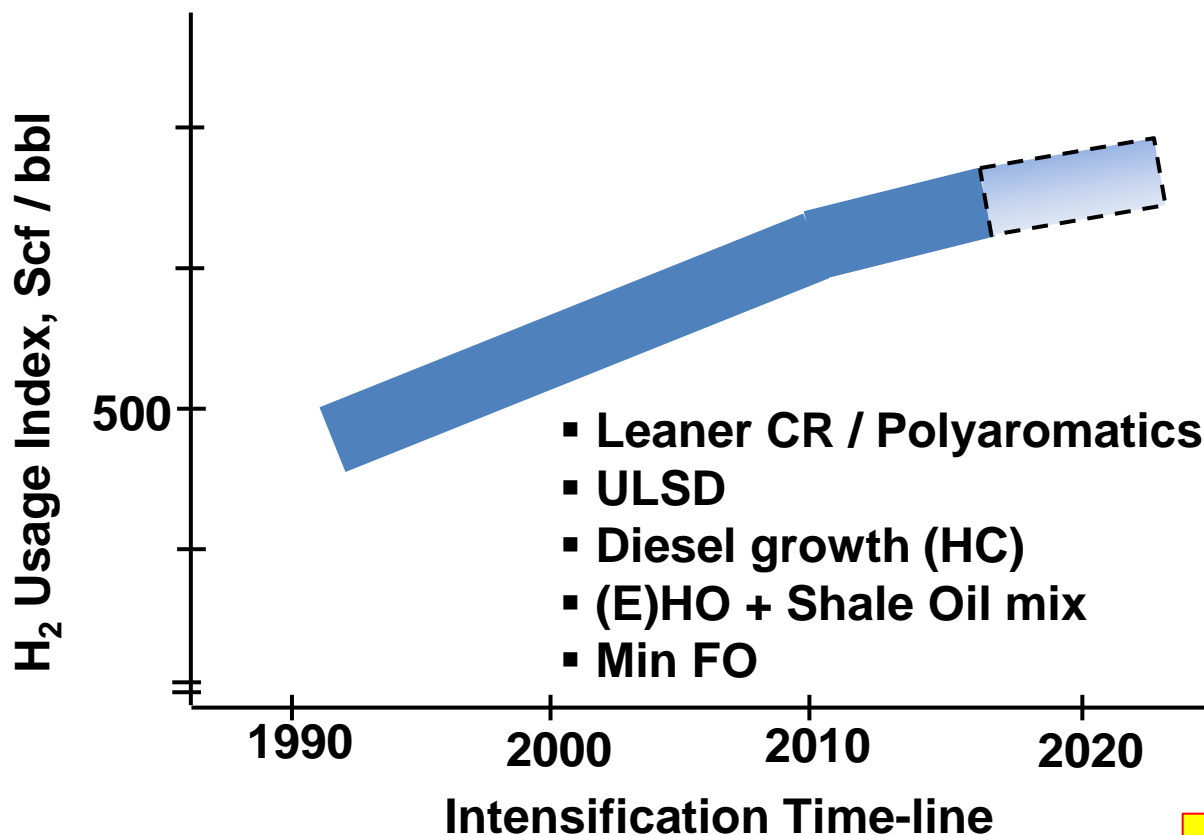
AFPM 2018 Annual Meeting New Orleans, USA; Mar 11-13



Presentation Outline

- Introduction
- Steam Reforming Pellet catalyst - status quo
- ZoneFlow™ (ZF) Reactor Technology - an innovative breakthrough
- ZF development status and validation programs
- Application of ZF Reactor Technology in hydrogen plants
 - ZF Single-Pass Reactors (ZF-SP)
 - Convective Pre-Reforming Reactors (ZF-CPR)
 - ZF Bayonet for Recuperative reforming (for New SMRs)

Introduction : Refinery Hydrogen Intensification



Projected CAGR : 3-4%
~ 0.8 BCfD

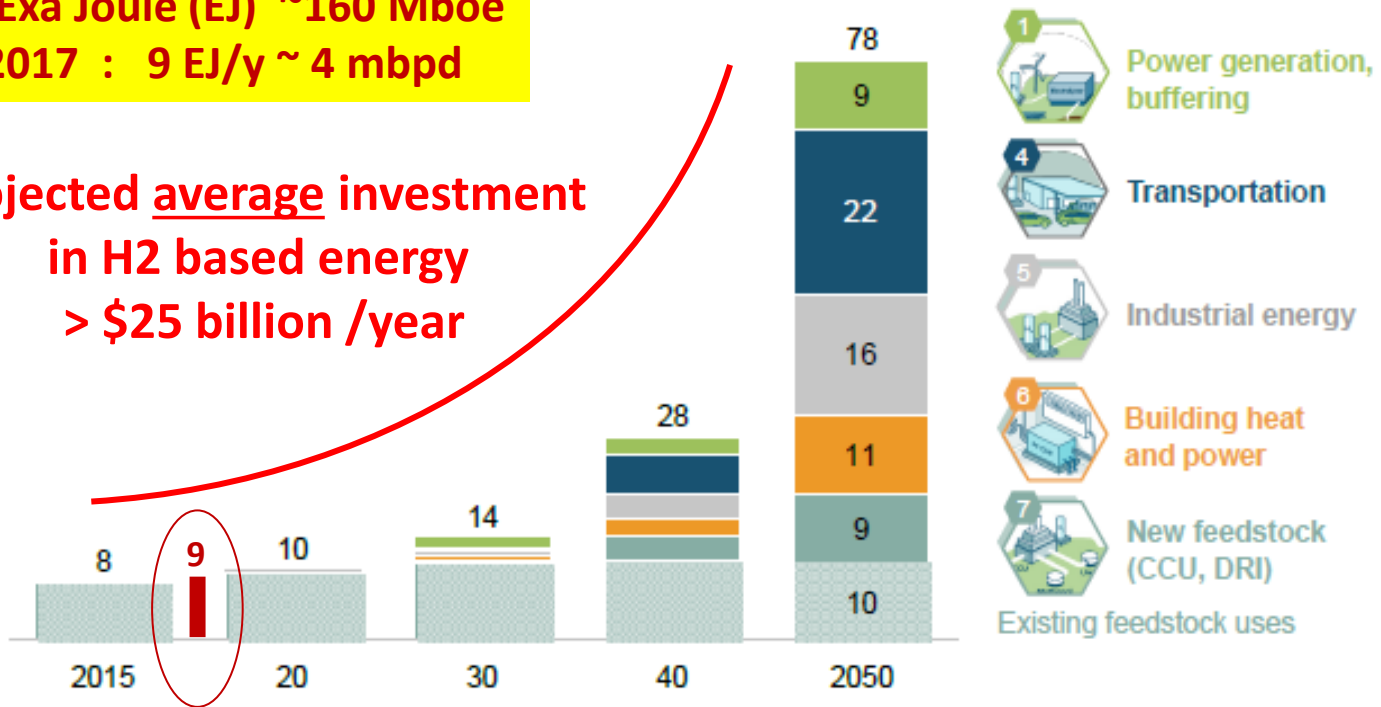
Hydrogen-for-Energy: Demand Projections (EJ)

Hydrogen demand could increase 10-fold by 2050

Global energy demand supplied with hydrogen, EJ

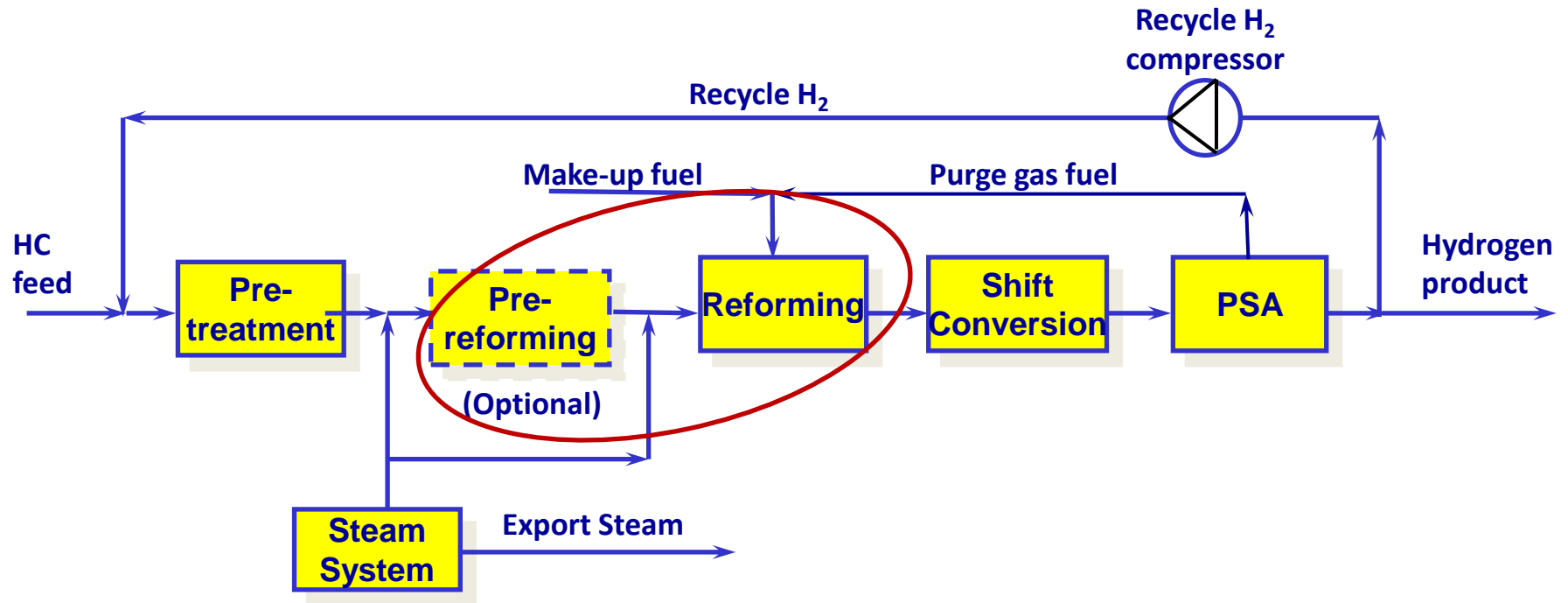
1 Exa Joule (EJ) ~160 Mboe
2017 : 9 EJ/y ~ 4 mbpd

Projected average investment
in H2 based energy
> \$25 billion /year



SOURCE: Hydrogen Council

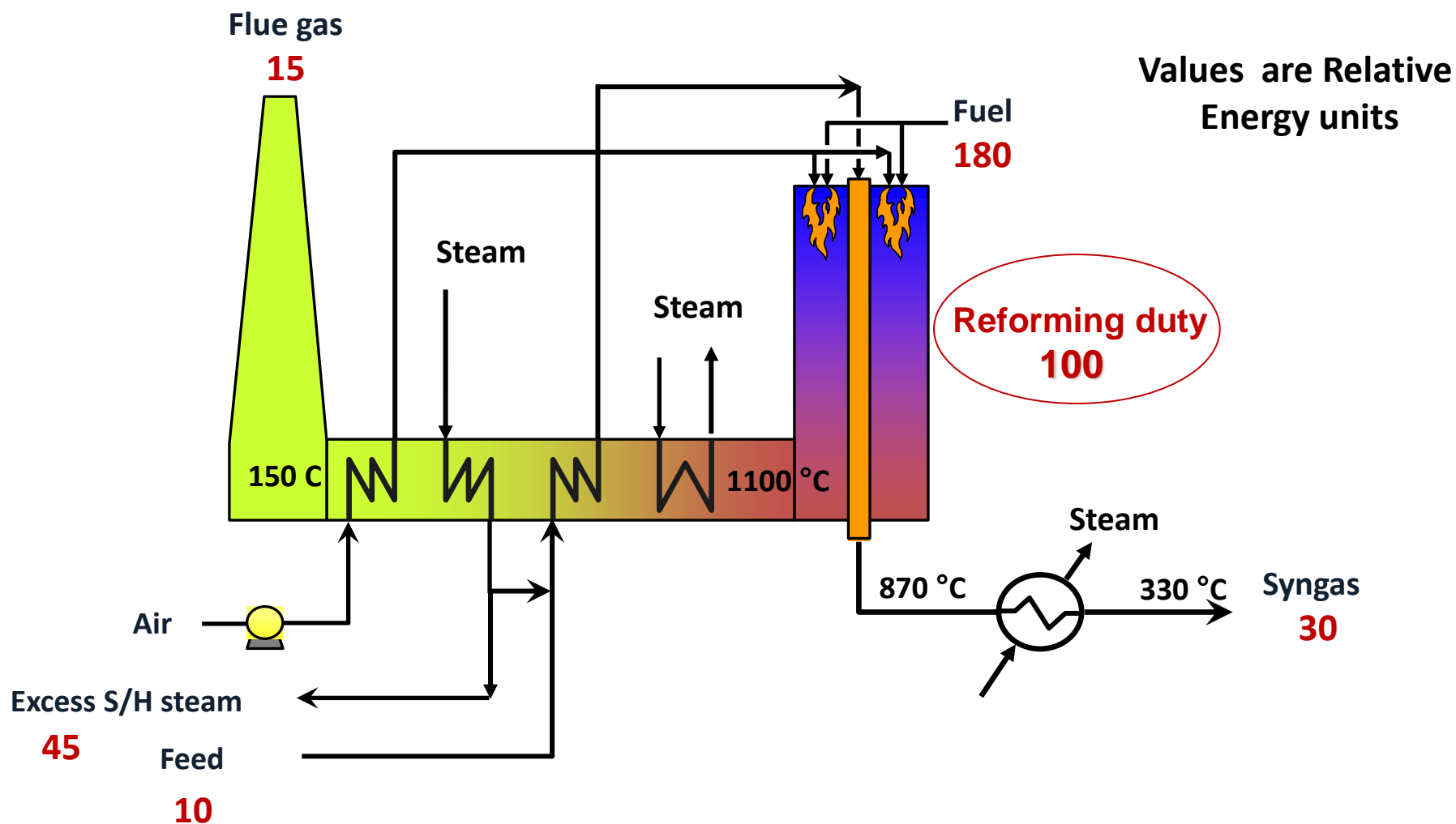
Typical Hydrogen Plant Block Diagram



40 → 400 → 600 → 900 → 350 → 40 Temp, C

Steam Reformer: Heart of Hydrogen Plant

Typical Overview



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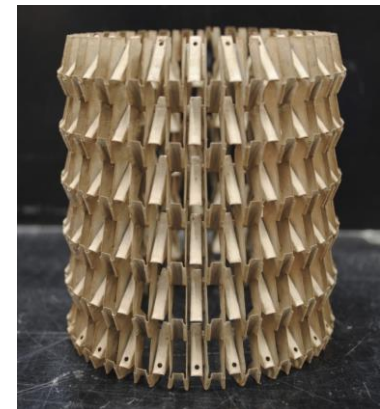
Steam Reforming Catalyst - Status Quo

- State-of-the-art steam reforming catalysts have by and large stayed “pellet-based” and so have the inherent deficiencies (of random packing) in terms of :
 - high pressure drop
 - limited heat transfer (sporadic catalyst-to-wall contact)
 - very low catalyst effectiveness (intrinsically diffusion limited)
 - catalyst attrition / breakage from thermal cycling
 - flow / temperature non-uniformity
- Various attempts for structured catalyst over the years, haven't been successful due to few core challenges

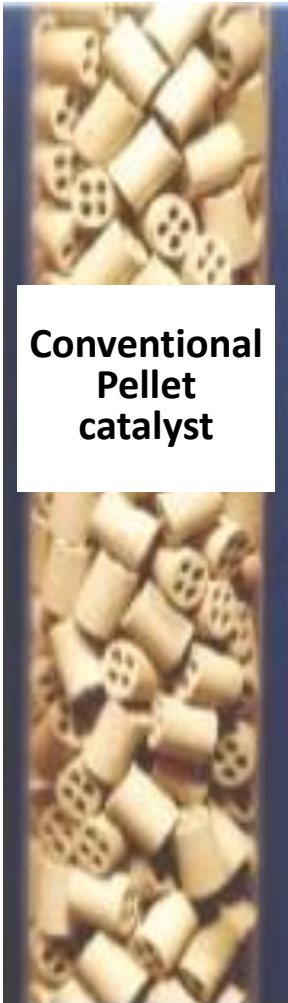
ZoneFlow Reactor Technology

– an Innovative Breakthrough

- Advanced high-performance structured catalyst with step improvements on key performance parameters, compared to current pellet catalysts :
 - up to 2 times higher heat transfer (including internal radiative transfer)
 - up to 50% lower pressure drop
 - annular flexible casing design ensures wall proximity in cold and hot conditions and also creates “near-wall” flow
 - up to 10 times higher catalyst effectiveness
 - high strength metal substrate; no attrition from thermal cycling
 - uniformity of flow over (longer) operating life
 - uniquely befitting for Recuperative reforming also



Conventional SMR Catalyst vs. ZoneFlow™ (ZF)



Conventional
Pellet
catalyst

- From random packing to uniform, engineered foil structure
- From irregular and scanty pellet-tubewall contact to uniform structure-to-wall contact in all conditions
- From strength-limited voidage and related flow resistance to robust high-voidage structure with near-wall turbulence



➤ ZF uniquely offers step-reduction in pressure drop combined with almost doubling of heat transfer coefficient



ZoneFlow™
structured
catalyst



Conventional SMR Catalyst vs. ZoneFlow™ (ZF)



Conventional
Pellet
catalyst



- From diffusion-limited active sites' access to high-GSA thin-fin structure with full surface access

High activity micro-layer catalyst with non-acidic and steam-stable substrate



➤ Multifold increase in catalyst effectiveness; higher resistance to coking and upsets; longer operating life

- From limited crush strength to durable & flexible metal structure



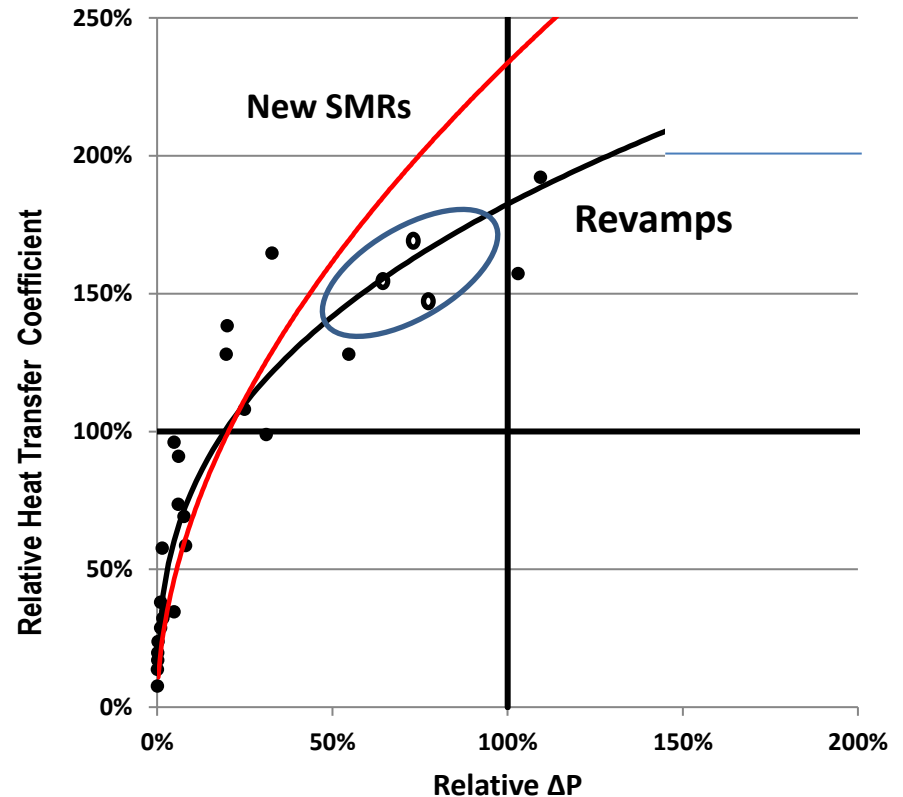
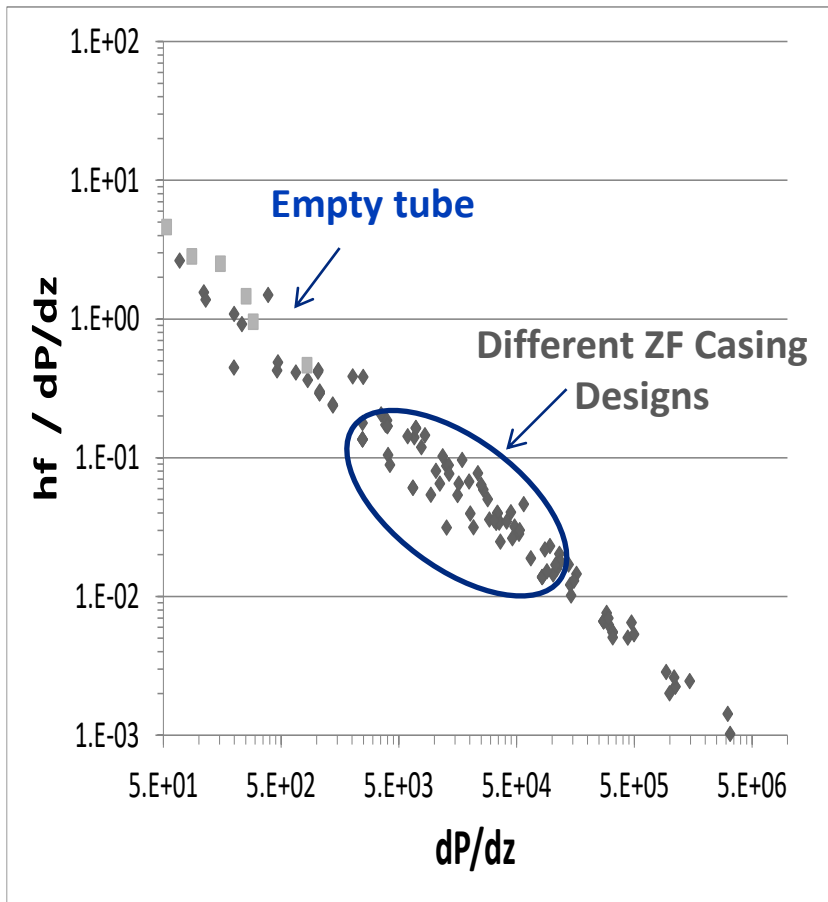
➤ No attrition or any breakage ; stable pressure drop and flow uniformity over full life



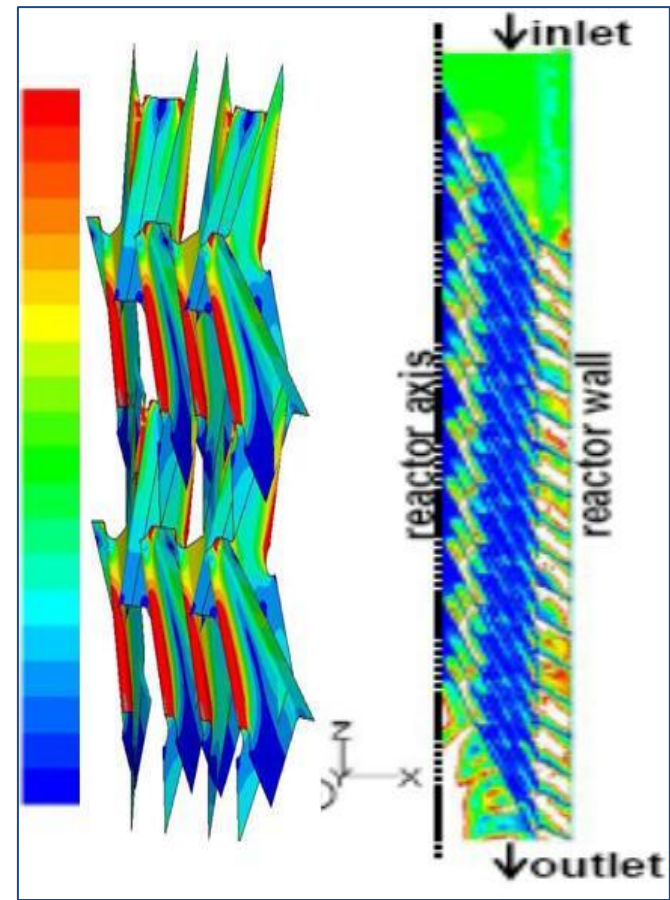
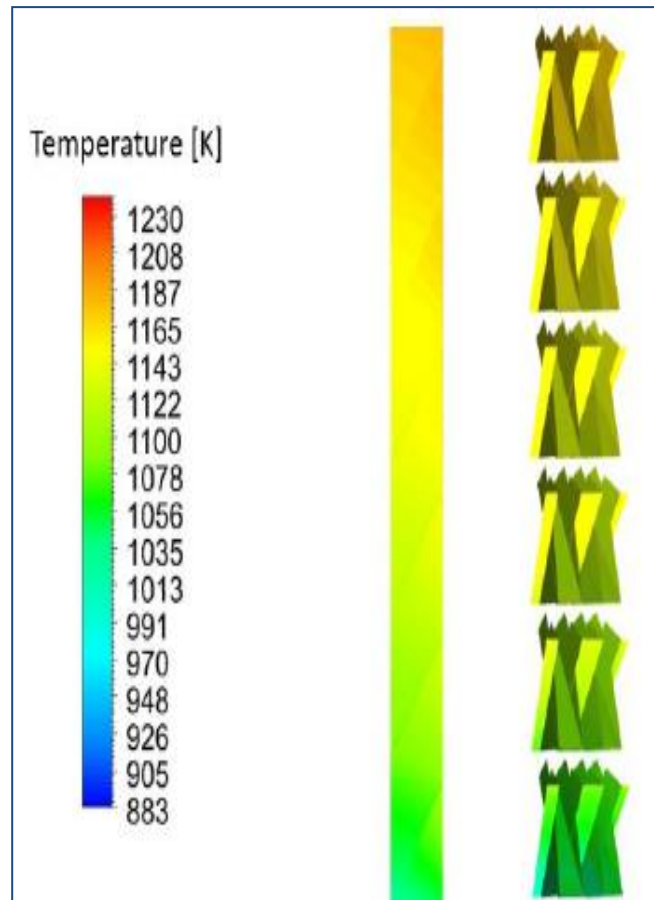
ZoneFlow™
structured
catalyst



ZF's Development : Detailed CFD Modeling



ZF's CFD Modeling and FE Analysis Results



ZF's Commercial Demonstration



Installation



Operation



Extraction

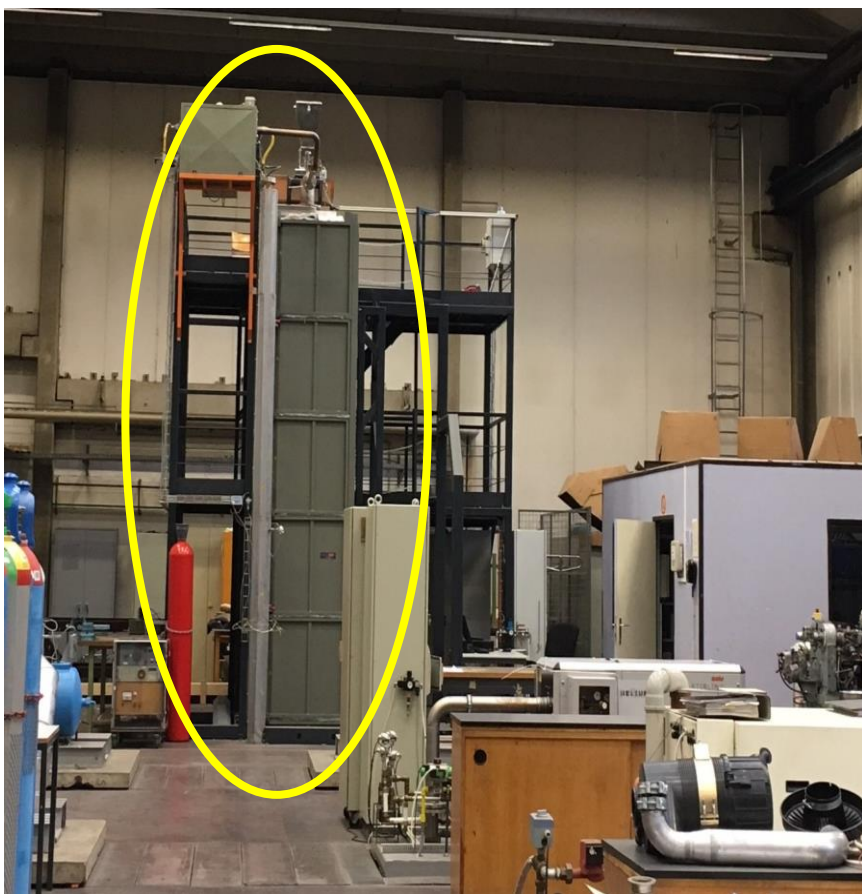
Demonstrated Results Compared to Pellet Tubes

- Up to 80° C lower TMT compared to adjacent tubes
- Up to 24% lower pressure drop
- No hot spots
- ZF structure intact in original form after >15,000 hrs operation and with 5 thermal cycles
- Lower S/C ratio operation was not available

ZFRT Pilot Plant

- At Université Catholique de Louvain (UCL), Belgium
- Fully equipped and instrumented pilot plant for extensive testing of ZF reactors under rigorous commercial conditions and beyond
- In collaboration with Prof. Gilbert Froment and Prof. Juray de Wilde
- Added micro-reactor lab for studying intrinsic reaction kinetics
- Operational 2Q 2018

ZFRT Pilot Plant Installation




ZF applications in (H₂)SMRs: Core-Merit Benefits

- ZF's lower dP, higher HTC and higher catalyst effectiveness allow the following underlying advantages, especially for retrofits :
 - higher throughput without increasing pressure drop
 - higher SMR outlet temp without increasing maximum tube skin temperature (TSM)
 - higher heat flux and/or higher reforming severity without increasing bridge-wall temperature and thus related firing / flue gas
 - lower approach to equilibrium
- Exploitation of ZF's annular structure supports "recuperating reforming"

ZF Solutions for Hydrogen SMRs

- **ZF-Single pass (ZF-SP)**
 - De-stressing and Retrofitting existing SMRs
 - Higher-flux, cost-effective and more reliable new SMRs
- **ZF-Convective pre-reforming (ZF-CPR)**
 - Unmatched in-situ retrofit for additional capacity in existing SMRs without major modifications
 - Efficient and cost-effective applications in new SMRs
- **ZF-Bayonet (ZF-B)**
 - Uniquely applicable for recuperative reforming in new SMRs, overcoming current challenges

ZF-SP for De-Stressing SMRs

- Stressed SMR Indicators / Attributes
 - Pressure drop (or its build up) limiting throughput
 - Loss of catalyst activity → hotter tubes limiting outlet temperature
 - Catalyst attrition / settling from thermal cycling
 - Carbon formation / hot spots
 - Impact on (remaining) tube life
 - Constrained reforming capacity
 - Replacing (pellet) catalyst in these SMRs with ZF-SP Reactors can overcome these deficiencies
- 

ZF-SP for De-Stressing of SMR

SMR De-Stressing	SMR Design	Stressed Operation	ZF-SP replacing pellets
Relative Capacity, %	100	95	100
Capacity limitations	-	dP, TSM	removed
S/C Ratio	3.0	3.3	2.8
Outlet temp, C	860	843	868
Approach to Equilibrium EOR C	-10	-12	-7
CH4 slip, dry vol %	5	5	5
Radiant Pressure drop, bar	2.8	2.8	2.3
Relative Radiant duty %	100	97	99
Avg heat flux kW/m2	78	74	78
Bridgwall temp, C	1000	980	998
TSM (avg) C	935	935	926

ZF-SP for De-bottlenecking or New SMR

- Achieve >5% more equivalent capacity
- Higher average heat flux (without exceeding tube design temperature)
- Improved temperature uniformity
- Extended tube life and improved reliability
- Extended EOR
- Optimized operation and enhanced reliability

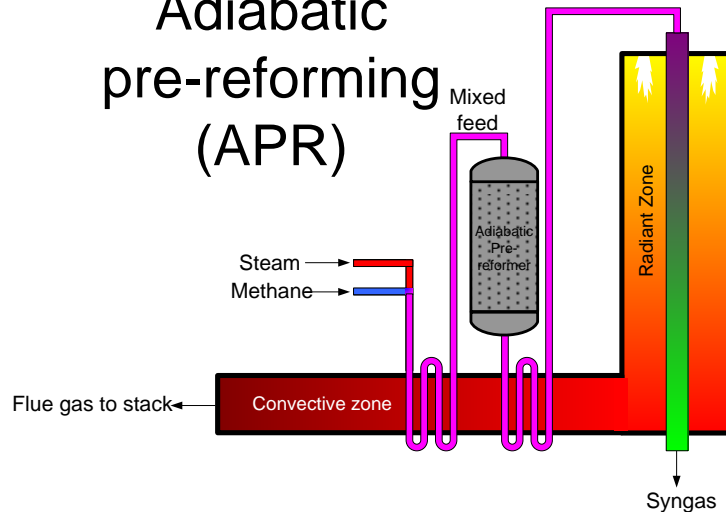
ZF-SP for Debottlenecking

		Reference	ZF-Radiant
Relative Capacity,	%	100	105
Capacity limitations		dP, TSM	removed
S/C Ratio		3.0	2.8
Outlet temp,	C	865	870
Approach to Equilibrium	C	-10	-7
CH4 slip,	vol %	5.5	5.7
Radiant Pressure drop,	bar	2.8	2.5
Relative Radiant duty	%	100	104
Avg heat flux	kW/m ²	75	78
Bridgwall temp,	C	1008	1004
TSM	C	940	938

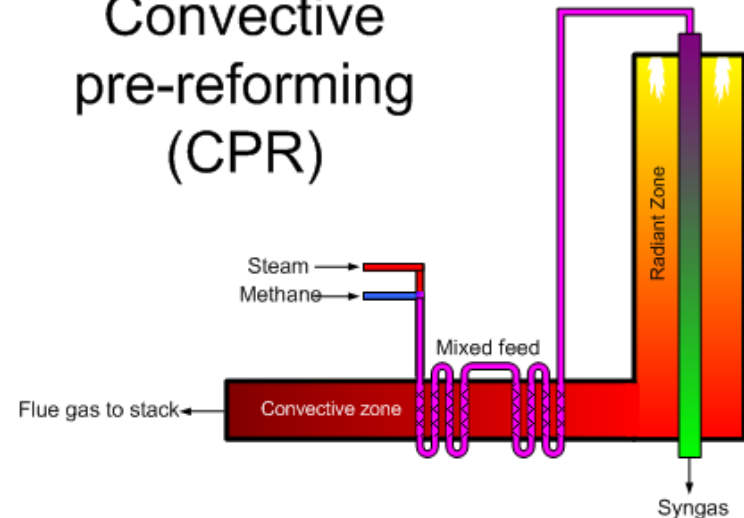
Pre-reforming

In-situ efficient use of higher grade
convective heat **using existing process coils**

Adiabatic pre-reforming (APR)



ZoneFlow™ Convective pre-reforming (CPR)



ZF Convective Pre-reforming (ZF-CPR)

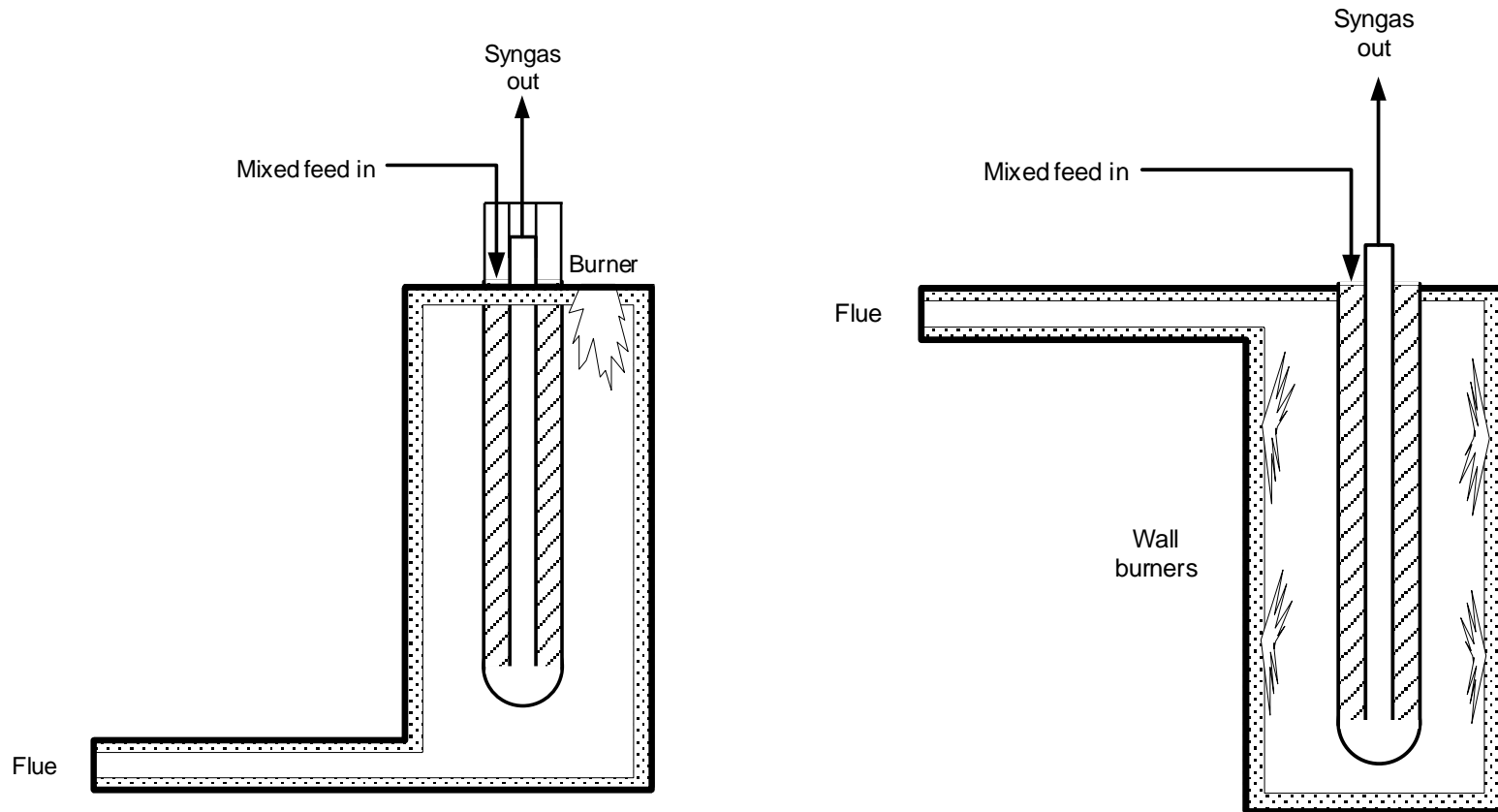
- Non-adiabatic convective pre-reforming using ZF-CPR inserts
- Tailored structured packing for very low dP, high GSA and (low temp reforming) activity
- **In-situ horizontal loading** in the mixed feed superheat coils
- Avoids major modifications and also the related downtime
- Optimization of pressure drop in combination with ZF-SP in SMR radiant tubes
- For revamps, 8-12% additional reforming without increasing SMR firing duty
- For New SMRs, 10-15% smaller SMR and proportionately also the steam system.

ZF-CPR for SMR Capacity Upgrade

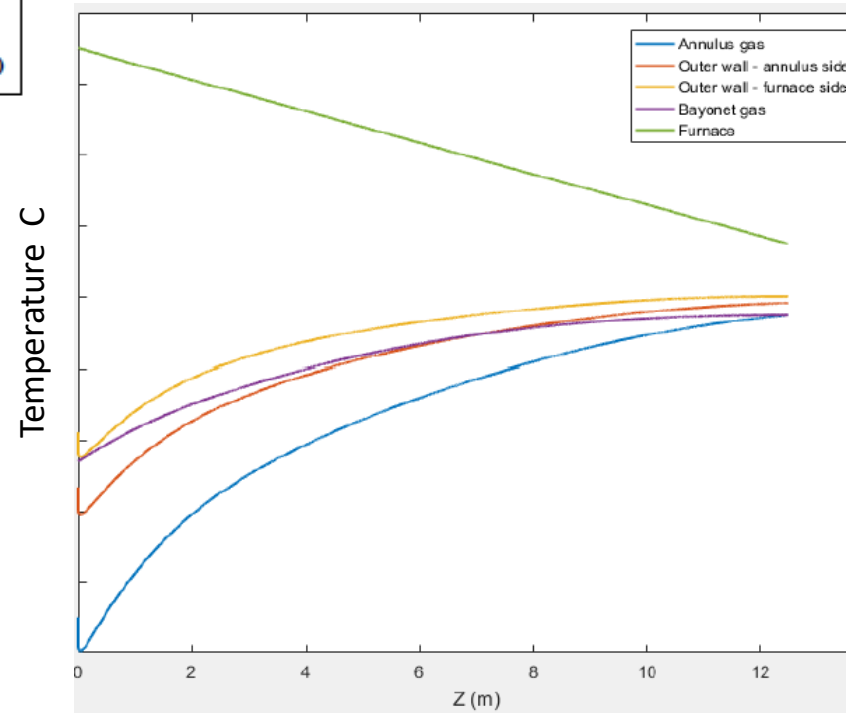
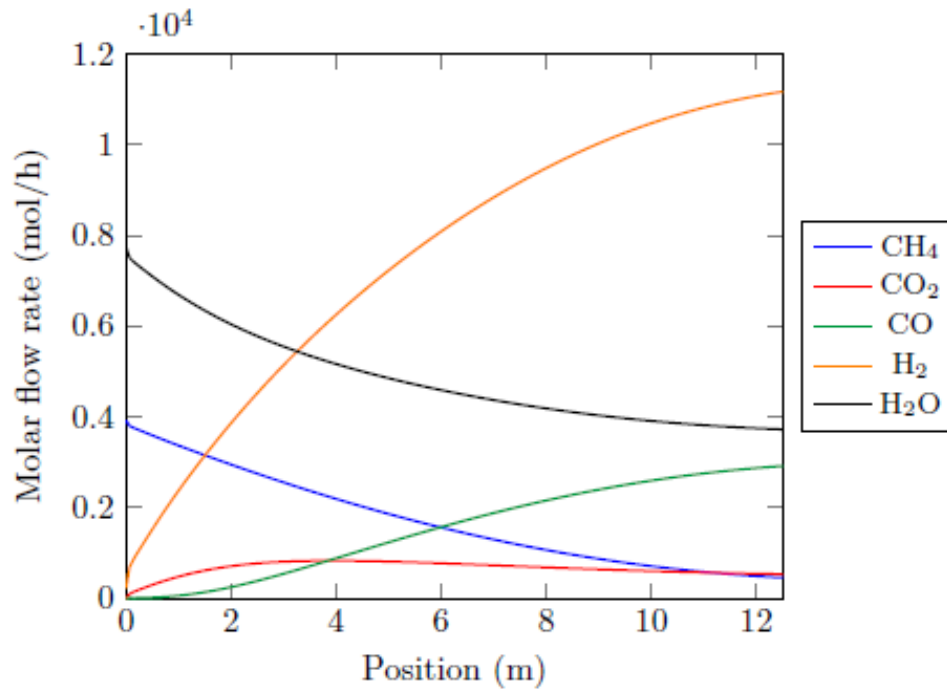
		Existing	ZF + CPR
Relative Capacity,	%	100	115
S/C Ratio		3.0	2.8
SMR inlet temp,	C	550	550 / 575 *
SMR outlet temp,	C	870	870 / 878 *
Approach to Equilibrium	EOR C	-10	-7
CH4 slip,	dry vol %	4.8	5.4 / 5.0
Radiant Pressure drop,	bar	2.5	2.3
Avg heat flux	kW/m2	80	80 - 82
Relative Radiant duty	%	100	100 / 103
Bridgewall temp,	C	1020	1009 / 1018
TSM	C	950	938 / 948

* Exploiting of existing plant design margins

ZF-Bayonet Configurations



ZF-Bayonet Modeling and Simulation Results



Drivers and Benefits of ZF-Bayonet

- Direct exploitation of ZF's inherent annular design
- Overcomes innate limitations of the “pellet” catalyst against crushing from differential expansion / thermal cycling
- SMR size reduction up to 20% based on high grade heat recovery for reforming
- Allows “Zero export steam” hydrogen plants for :
 - remote, stand-alone or “distributed ” hydrogen plants not having a steam host
 - cases where export steam has low or no credit compared to fuel
- Allows lowering of carbon-footprint from reduced firing per unit H₂
- Compact / modularized SMR units
- Applicable in various SMR configurations and designs

Conclusions

- Hydrogen demand growth projections are strongly encouraging
- Steam reformer is the heart of an H₂ plant; its performance and tube life are governed by catalyst
- Current pellet catalysts have inherent deficiencies, thus limiting the extent of possible improvements.
- ZoneFlow Reactor Technologies (ZFRT) has developed an innovative structured catalyst
- Exceptional and advanced solutions for revamping as well as new hydrogen SMRs, offering OPEX and CAPEX benefits.
- Successful demonstrations and pilot plant for testing under commercial / client-specific conditions



ZoneFlow Reactor Technologies, LLC

Thank You !

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